

# Seminar: Efficient Triple-Energy Outlook and Practices to manage UK's 10-40 TWh of industrial waste heat



Organiser: Energy Institute (EI) North Eastern Branch

Sir Joseph Swan Centre for Energy Research

Date: 11th December, 2013

Time: 2:00 – 3:30pm

Venue: Old Library, Newcastle University, NE1 7RU, UK

# Cogeneration of Cooling and Electricity by Low Grade Heat

Low grade heat driven adsorption-linear-expander  
cycle for cogeneration of power and refrigeration

( EPSRC - LH Cogen )



Sir Joseph  
Swan Centre  
for energy research

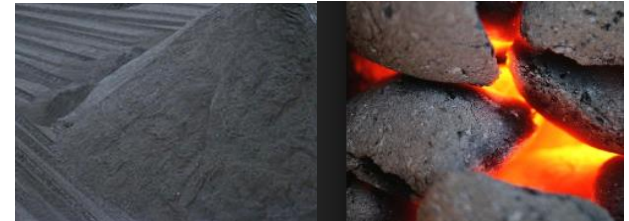
Dr Yaodong Wang

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- 2 Design and manufacture of LH Cogen system
- 3 Experimental studies and modelling analysis
- 4 Improvement and potential applications
- 5 Conclusions

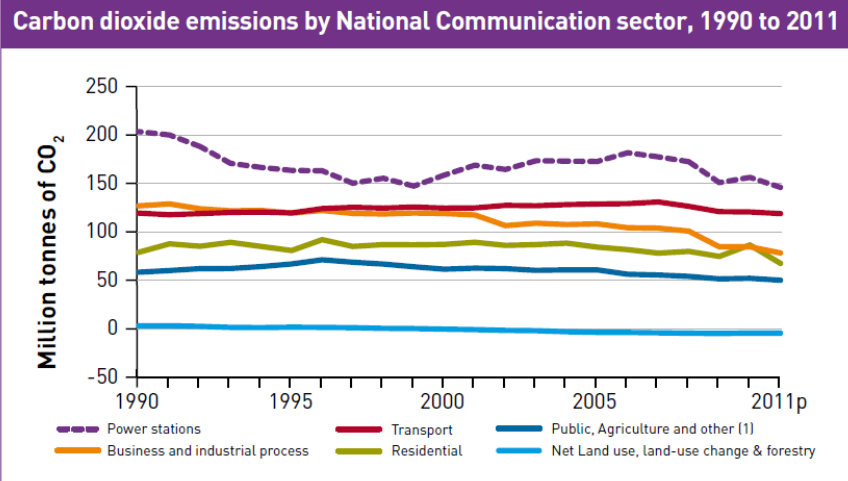
# 1. Background

This research project is highly relevant to the priority areas of Energy and Environmental Change issues.

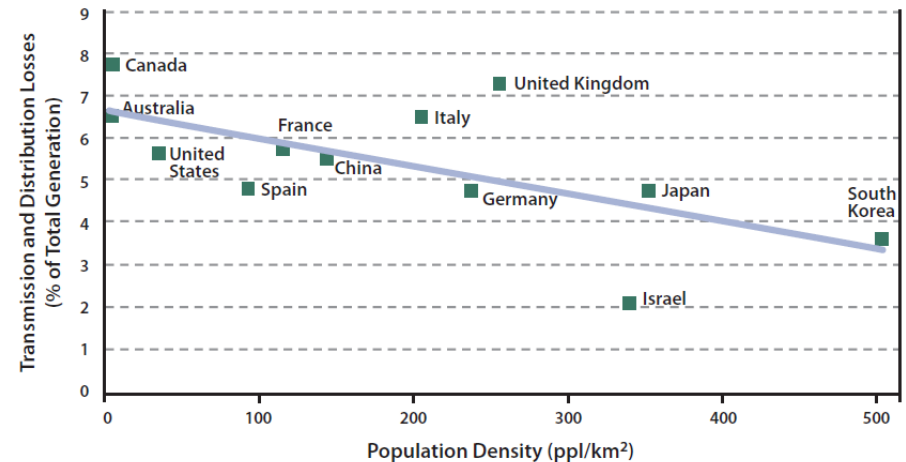


Fossil fuels are the main sources of energy we use today

- In UK, the final energy consumption in 2011: **211.7** million tonnes of oil equivalent;
- **18.5%** of the final energy consumed by electricity generation industry
- their average thermal efficiency was **36.8%**;
- **11.7%** of the final energy consumption (**24.75** million tonnes of oil equivalent) was wasted in the form of low grade heat.

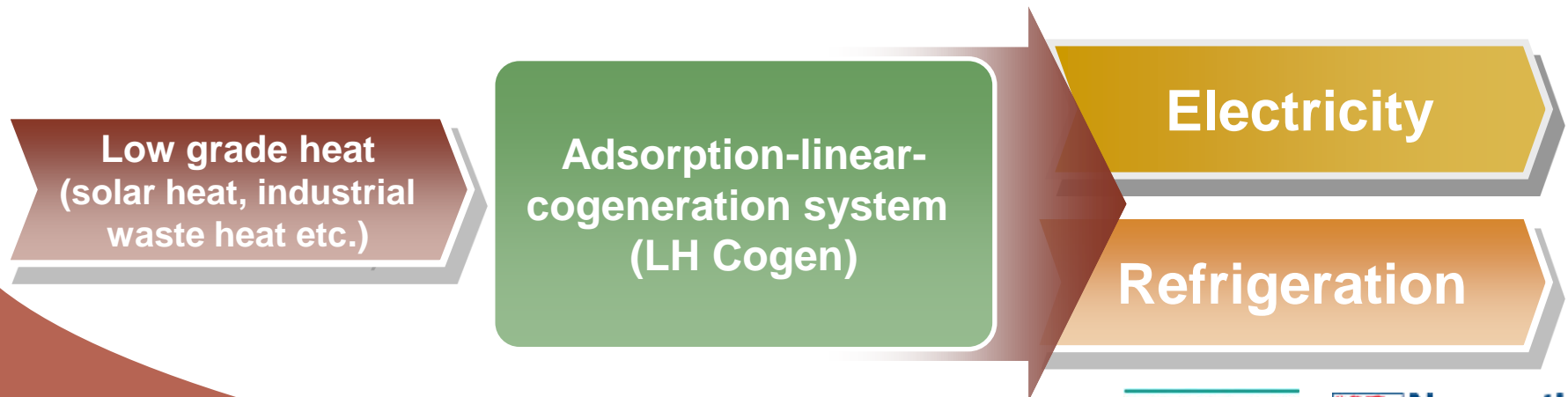


**Figure 1.5 Transmission and Distribution Losses for Selected Countries, 2008**



## LH Cogen system (Low grade heat driven adsorption-linear-expander cycle for cogeneration of power and refrigeration)

- driven by *low grade heat*, avoiding primary energy consumption, increasing the energy utilisation efficiency;
- using *ammonia* as refrigerant (zero GWP and zero ODP), environmental friendly;
- cogeneration of refrigeration and electricity (*a variety of cooling levels*)
- *Competitiveness* with conventional power/cooling cogeneration technologies: Goswami cycle and APC cycle (absorption power/cooling combined cycle)



# Absorption/Adsorption

- Thermally driven refrigeration: absorption/adsorption
- Refrigerant: ammonia ( $\text{NH}_3$ ), water ( $\text{H}_2\text{O}$ ), methanol ( $\text{CH}_4\text{O}$ ), lithium bromide ( $\text{LiBr}$ )...
- Ammonia:
  - ✓ Zero ODP, zero GWP
  - ✓ the most cost effective and energy efficient method of processing and storing frozen and unfrozen foods
  - ✓ its distinctive smell is detectable at concentrations (5 ppm) well below those considered to be dangerous (35 ppm limitation for short term exposure about 15 minutes )
  - ✓ lighter than air
  - ✓ BREEAM, UNEP, ASHRAE etc. have given decent credits to ammonia

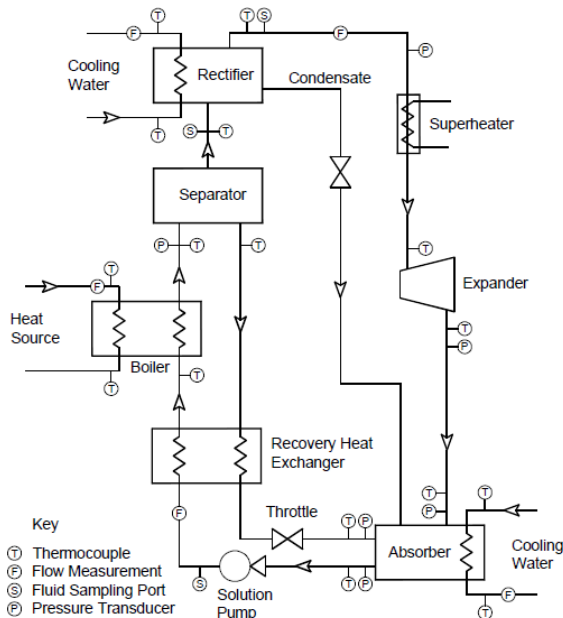
# Goswami cogeneration cycle

## ➤ absorption-basis cogeneration cycle)

- proposed by Goswami in 1995 based on Kalina cycle
- the binary mixture of ammonia and water
- Cooling effect extracted from the exhausted low temperature vapor of the turbine (sensible heat)
- Low or medium heat source from 80 to 200 °C: thermal efficiency of cooling (COP) 0.01 ~ 0.06; thermal efficiency of power generation 0.05 ~ 0.10.
- So far no practical application

## ➤ Drawbacks compared with LH Cogen cycle

- Require more complex parts, such as liquid pump or rectifier or separator)
- Limited range of heat source
- Low refrigeration COP : the working fluid at the exit of the turbine likely remained as wet vapour

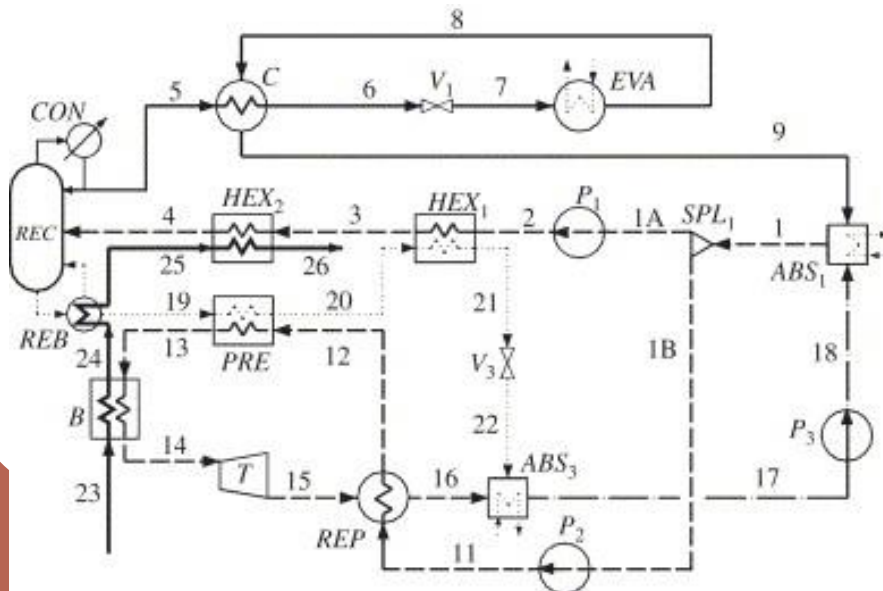




# APC cycle

## ➤ Ammonia absorption power/cooling combined cycle (APC)

- an improved Goswami cycle, employing a throttle valve to ensure the sub-cooling state before vaporisation,
- Much more complex system
- Medium heat source from 200 °C to 450 °C: thermal efficiency of cooling and power was 0.06 and 0.21 with 450 °C heat source.
- So far no practical application



## ➤ Drawbacks compared with LH Cogen cycle

- Require more complex parts, such as liquid pump or rectifier or separator, throttle valve
- the complex design compromises the compactness
- Low refrigeration COP

# LH Cogen cycle

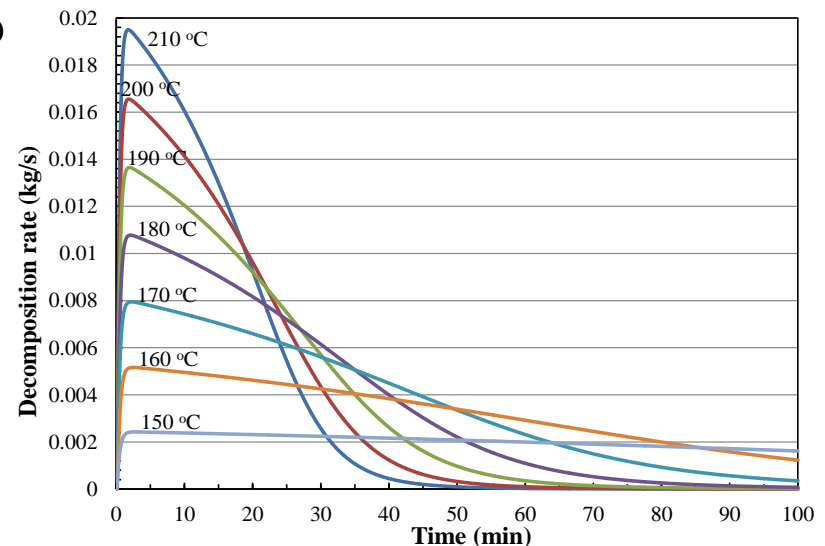
## ➤ LH Cogen (adsorption-basis cogeneration cycle)

Inherits the merits of adsorption over absorption

- a wider range of thermal energy utilisation, 50 ~ 600 °C  
(NiCl<sub>2</sub>/MnCl<sub>2</sub>/BaCl<sub>2</sub>/CaCl<sub>2</sub>/MgCl<sub>2</sub>/NaBr/SiCl<sub>2</sub>.....)
- a much simpler construction requiring easier operation and maintenance  
( no liquid pump or rectifier or separator for refrigerant)
- Evaporation refrigeration (latent heat), ideal COP as 0.4 (Goswami and APC < 0.1), ideal thermal efficiency of p

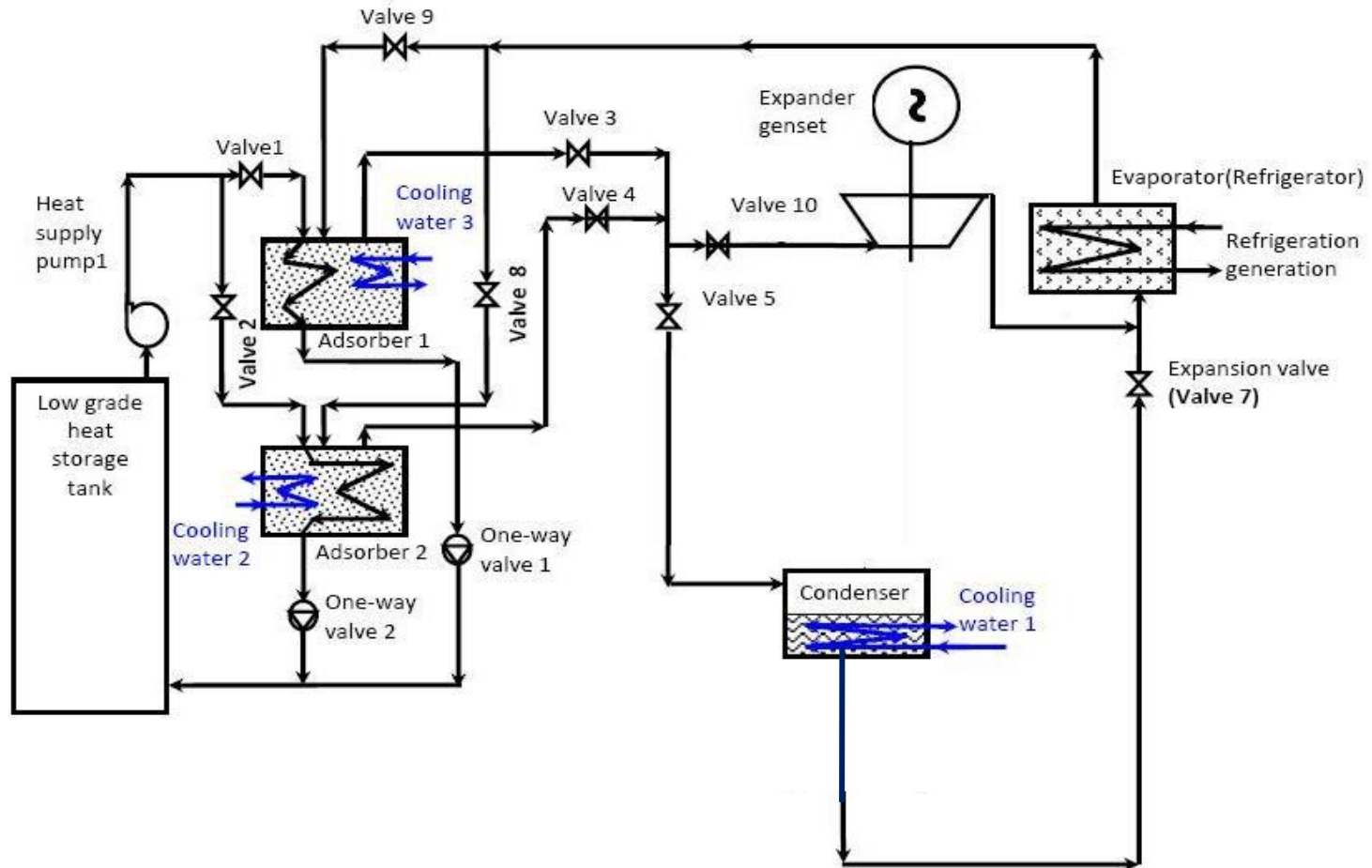
## ➤ Drawbacks compared others

- Natural Intermittence
- Relatively unstable reaction rate, impact on the expander performance.



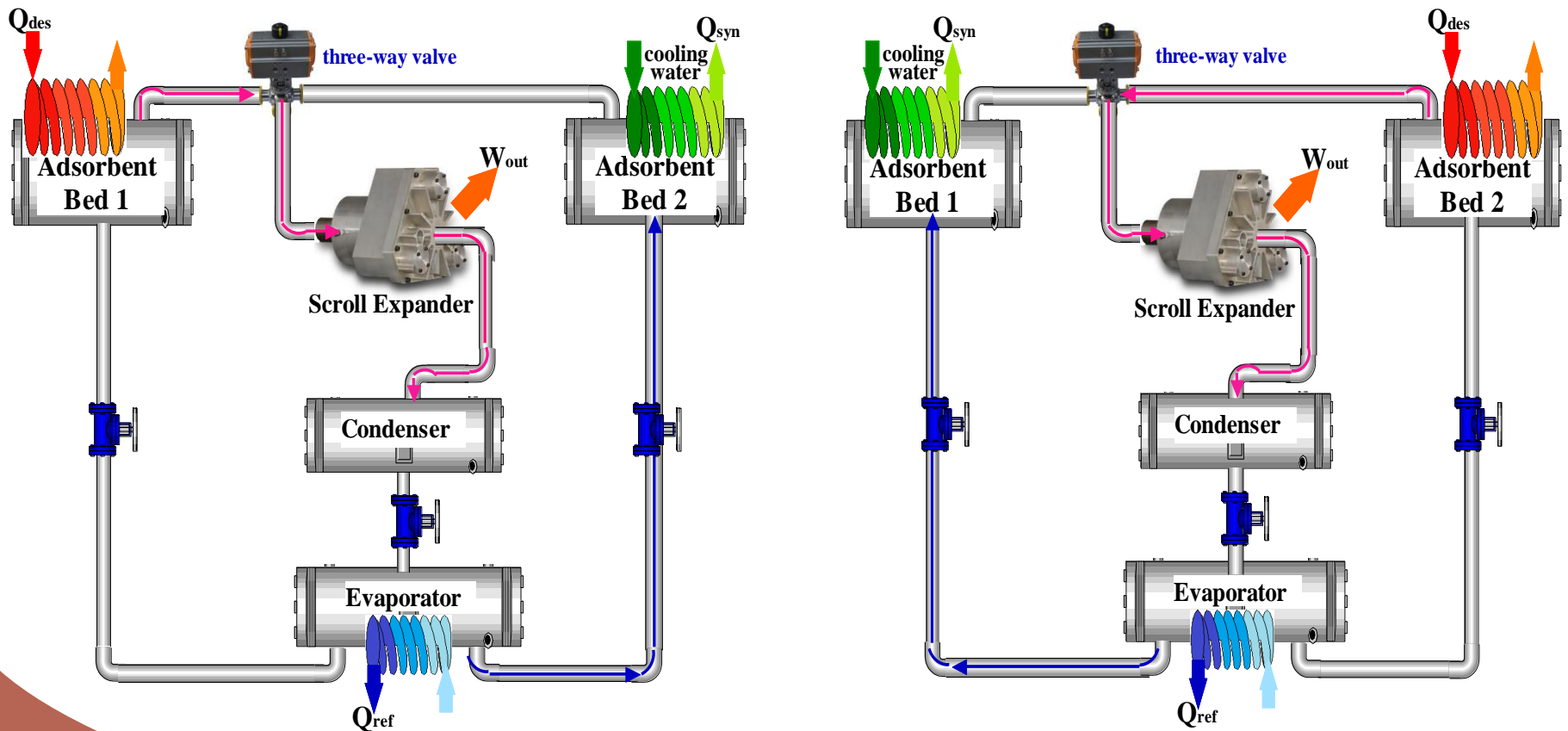
## 2. Design and manufacture of LH Cogen system

### Principle of LH Cogen system

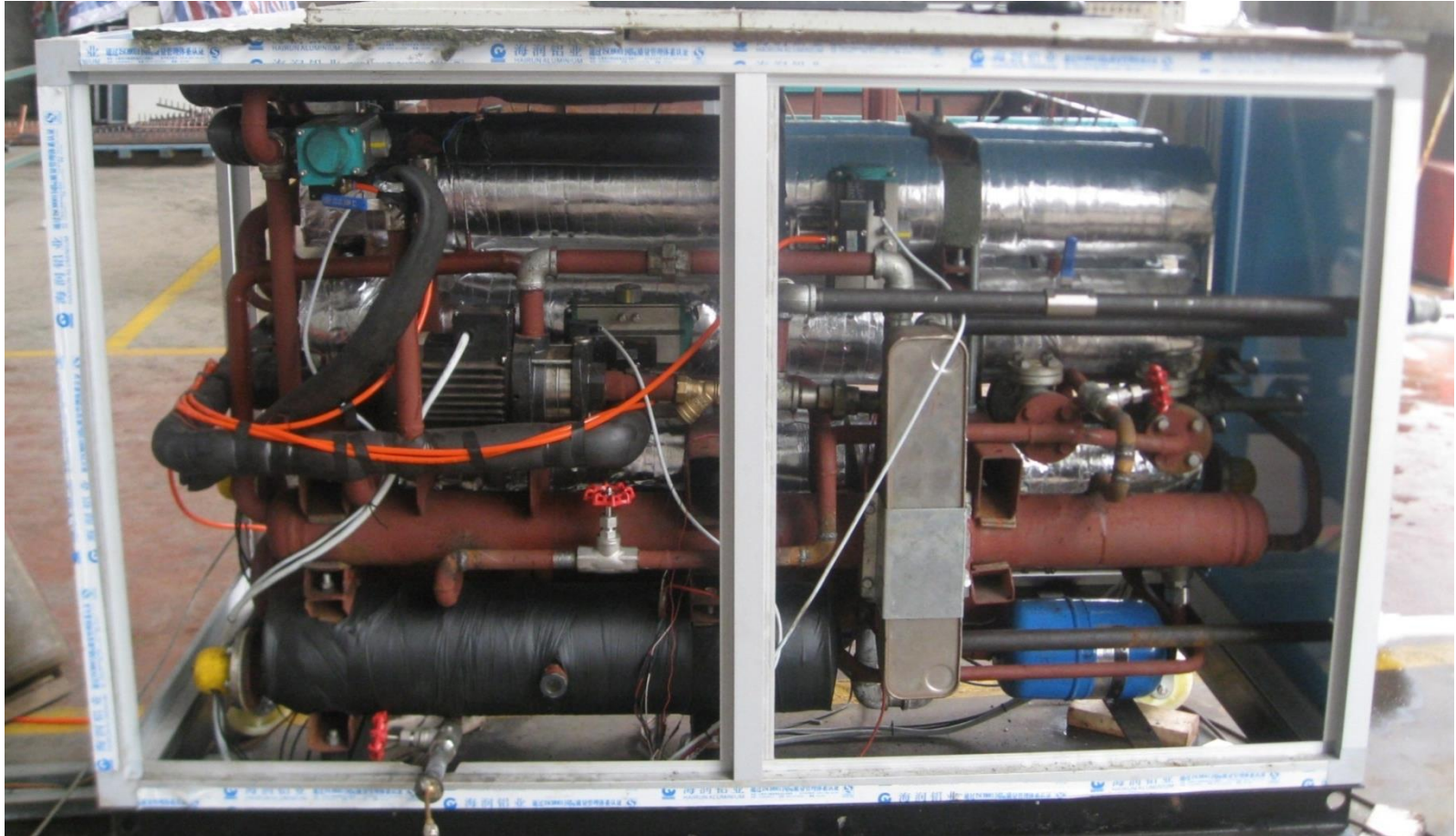


# Principle of LH Cogen system

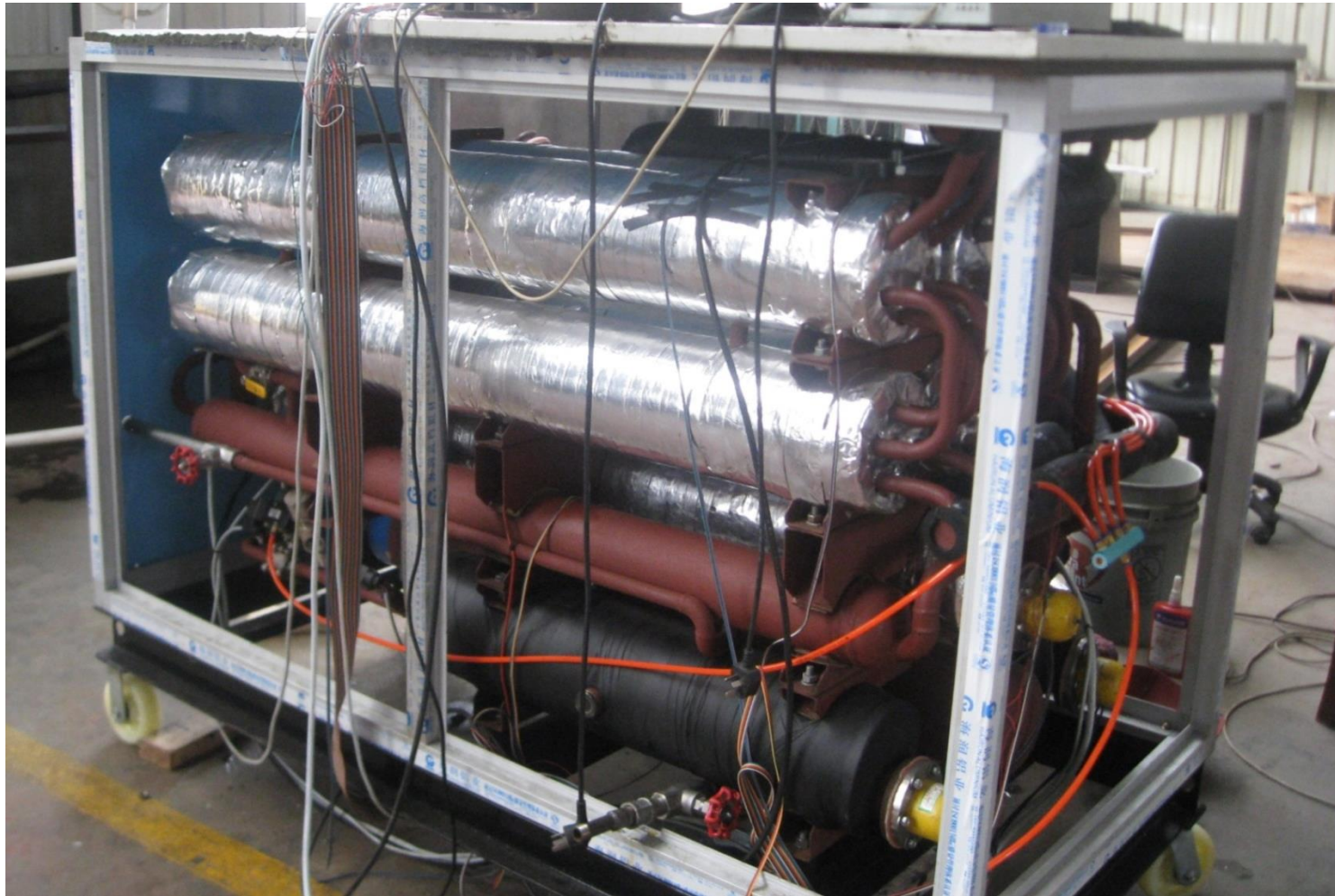
two sets of adsorption cycle are working out-of-phase to overcome the intermittence of adsorption



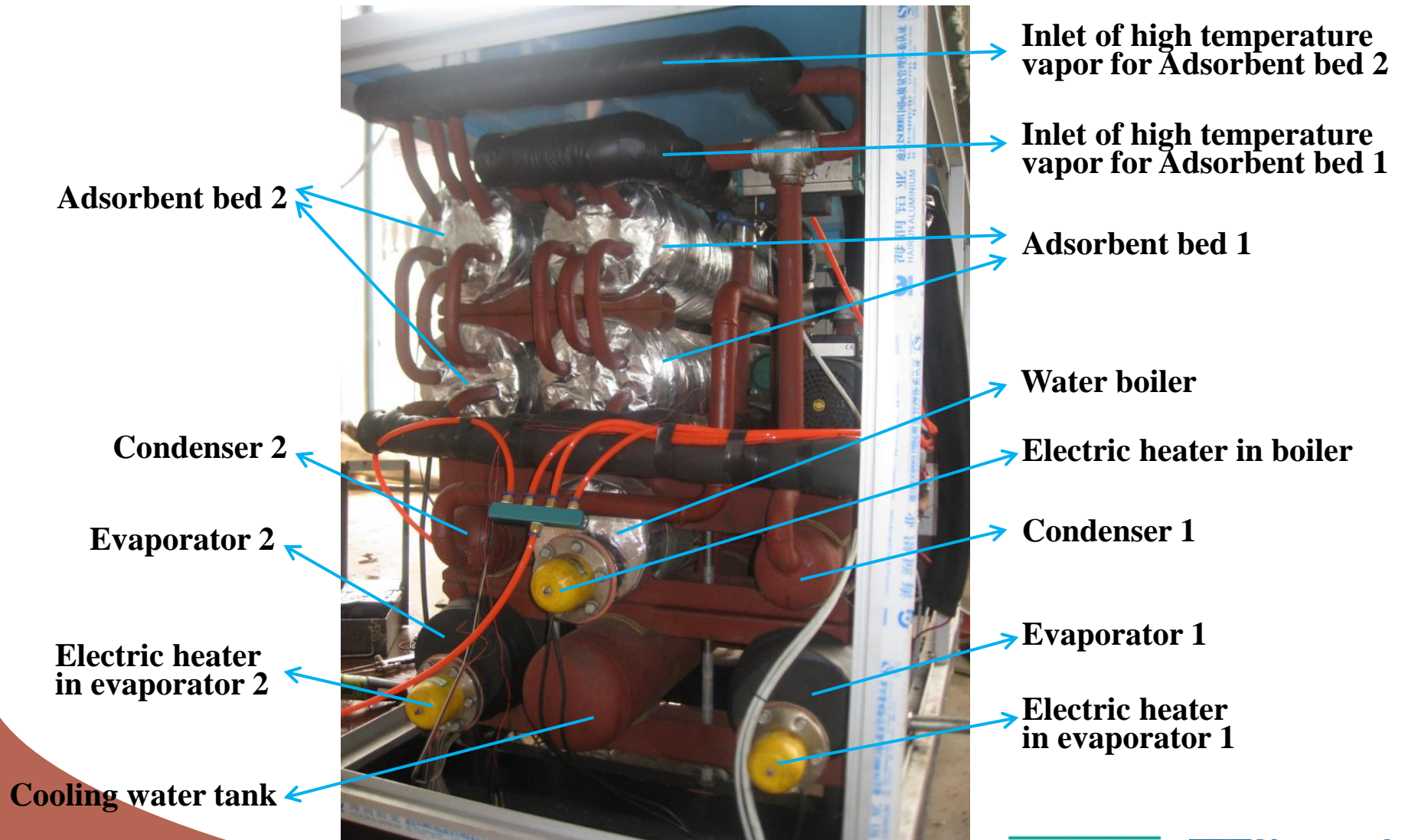
# Photos of adsorption chiller



# Photos of adsorption chiller



# Components of the chiller



# 3. Experimental studies and modelling analysis

## Experimental setup



Adsorption chiller



Cooling tower



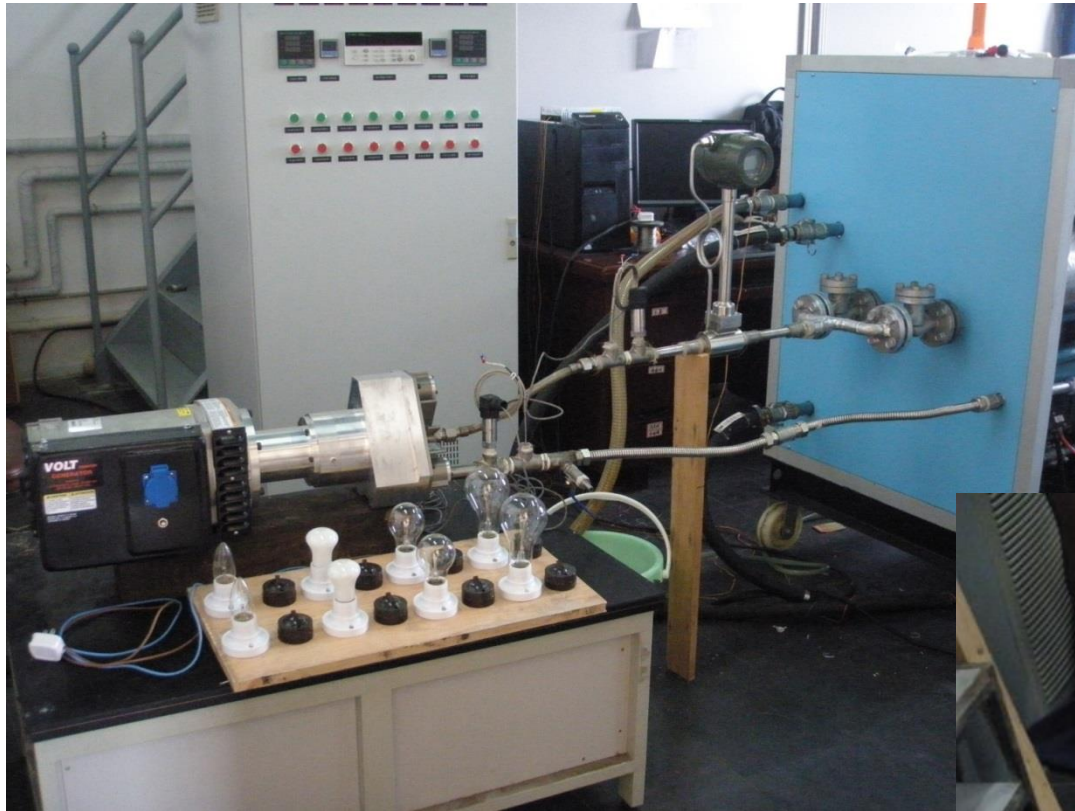
Data collection devices



Control panel of chiller



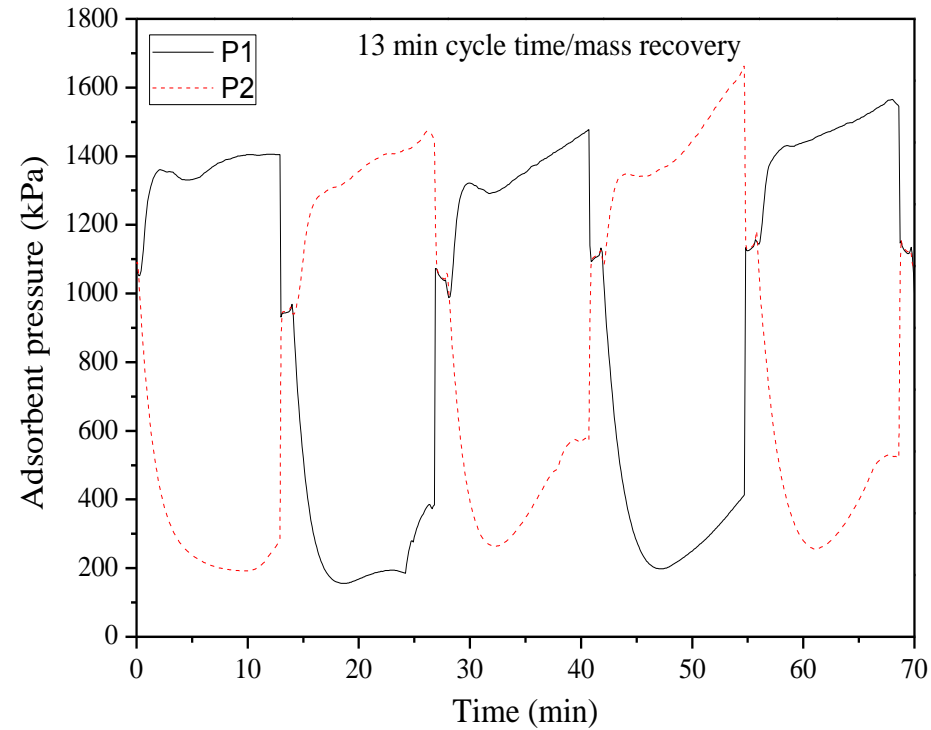
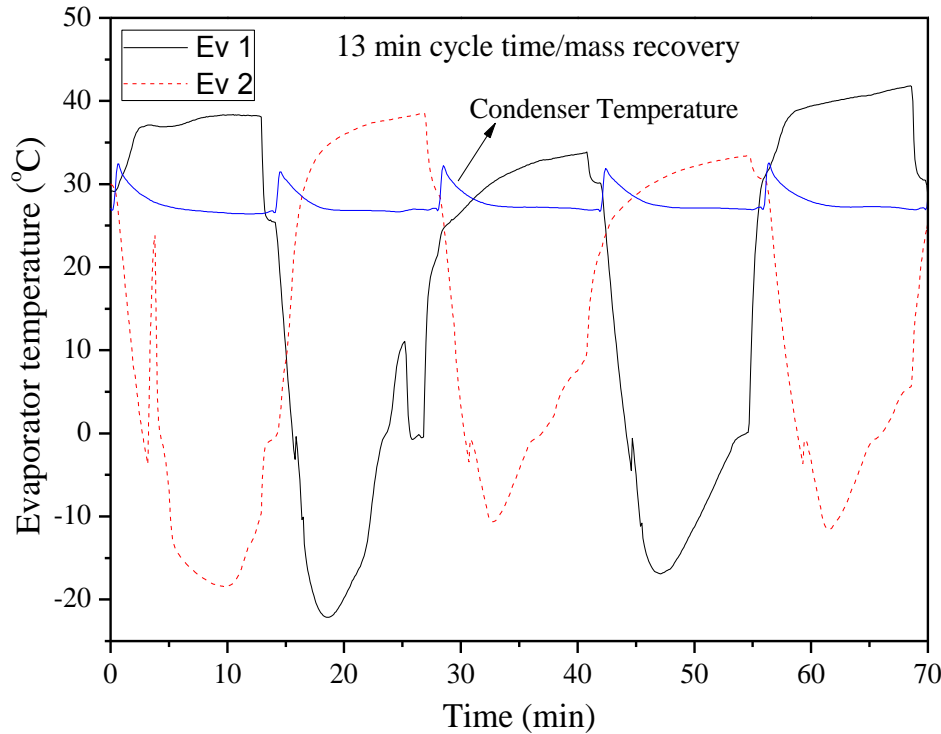
# Integration with scroll expander



Light bulbs as load bank

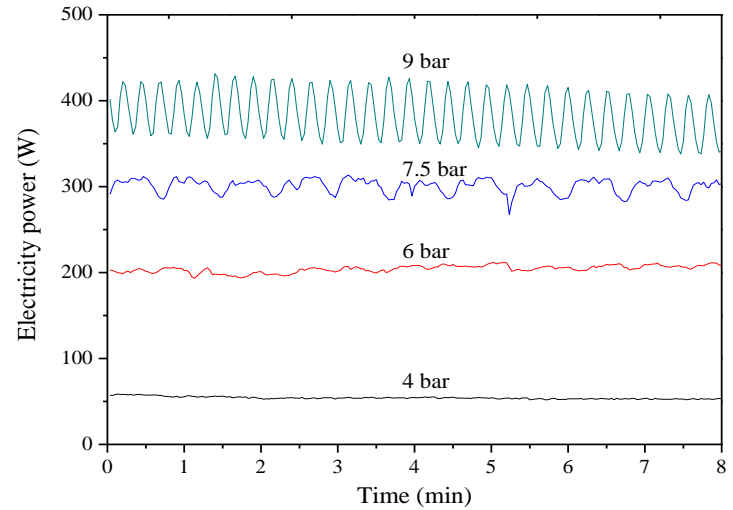
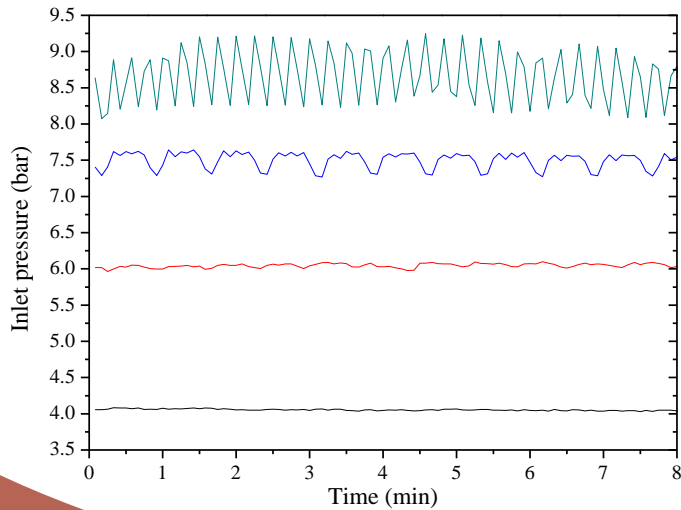
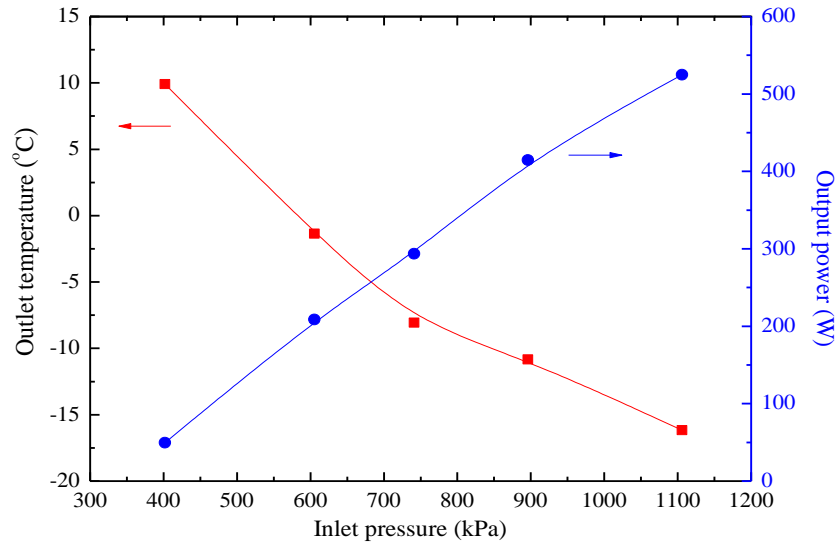


# Result: Adsorption chiller performance

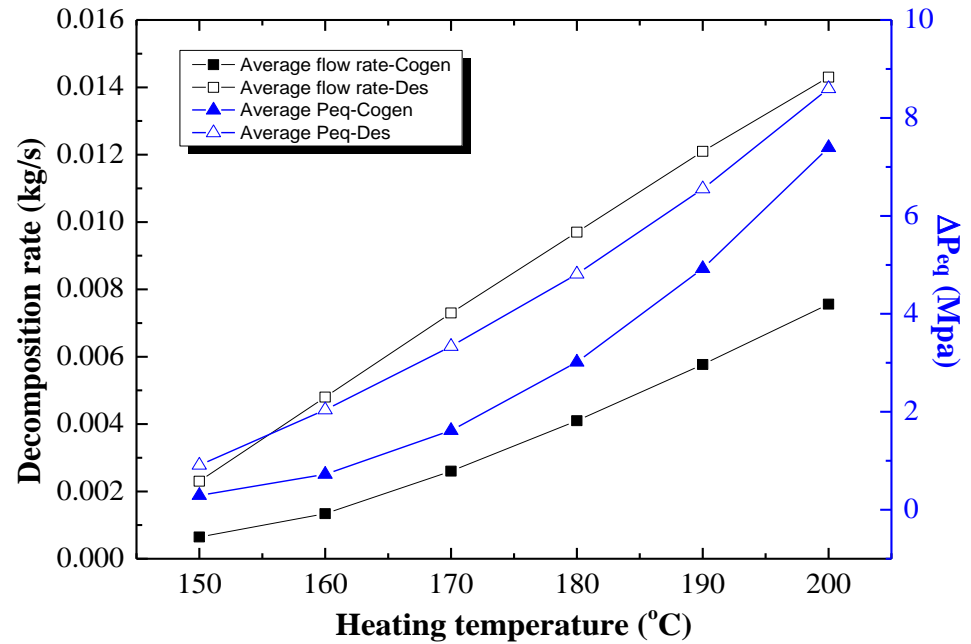
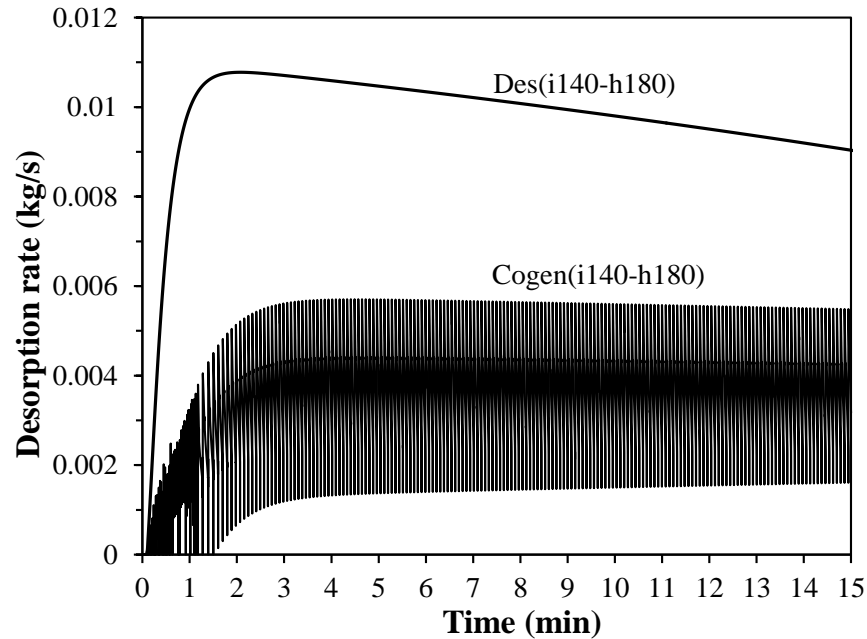


	Cycle time (min)	Average heating temperature (°C)	Average refrigeration temperature (°C)	Average cooling power (W)	COP
MR	13	125	-2.50	3190	0.20
Non- MR	13	126	-0.02	2090	0.14
MR	26	124	-0.80	2410	0.14

# Result: Scroll expander performance

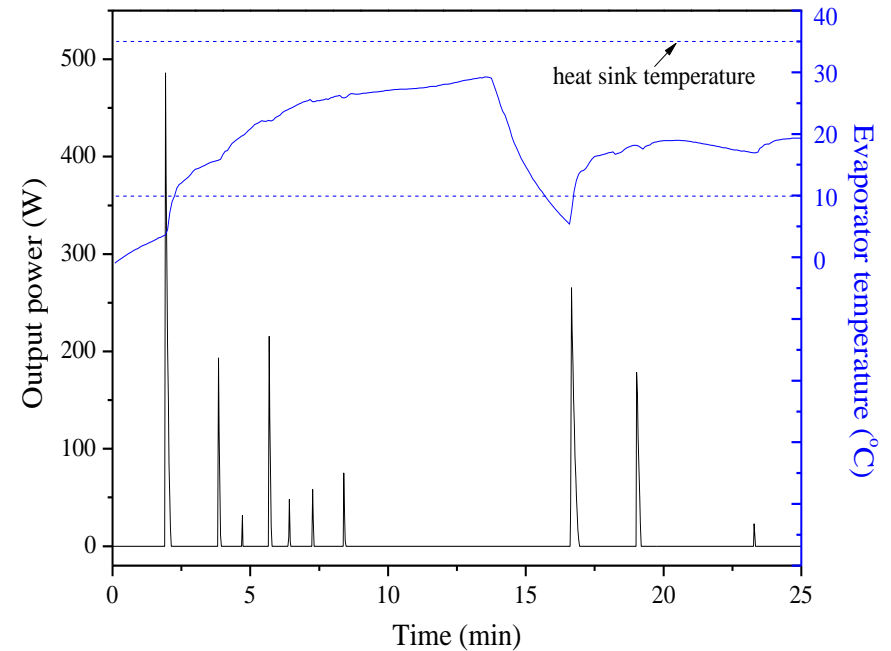
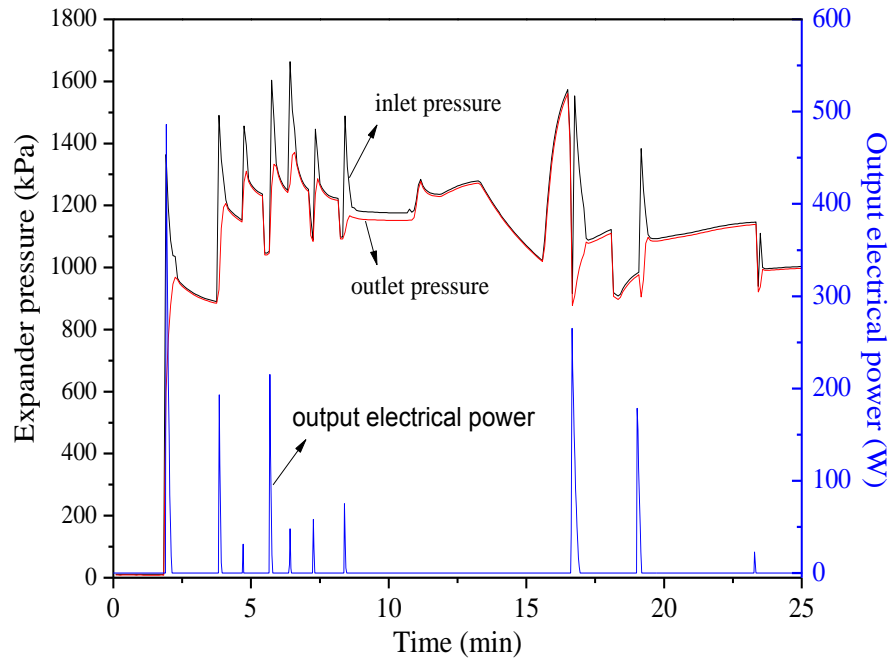


# Result: Modelling simulation analysis

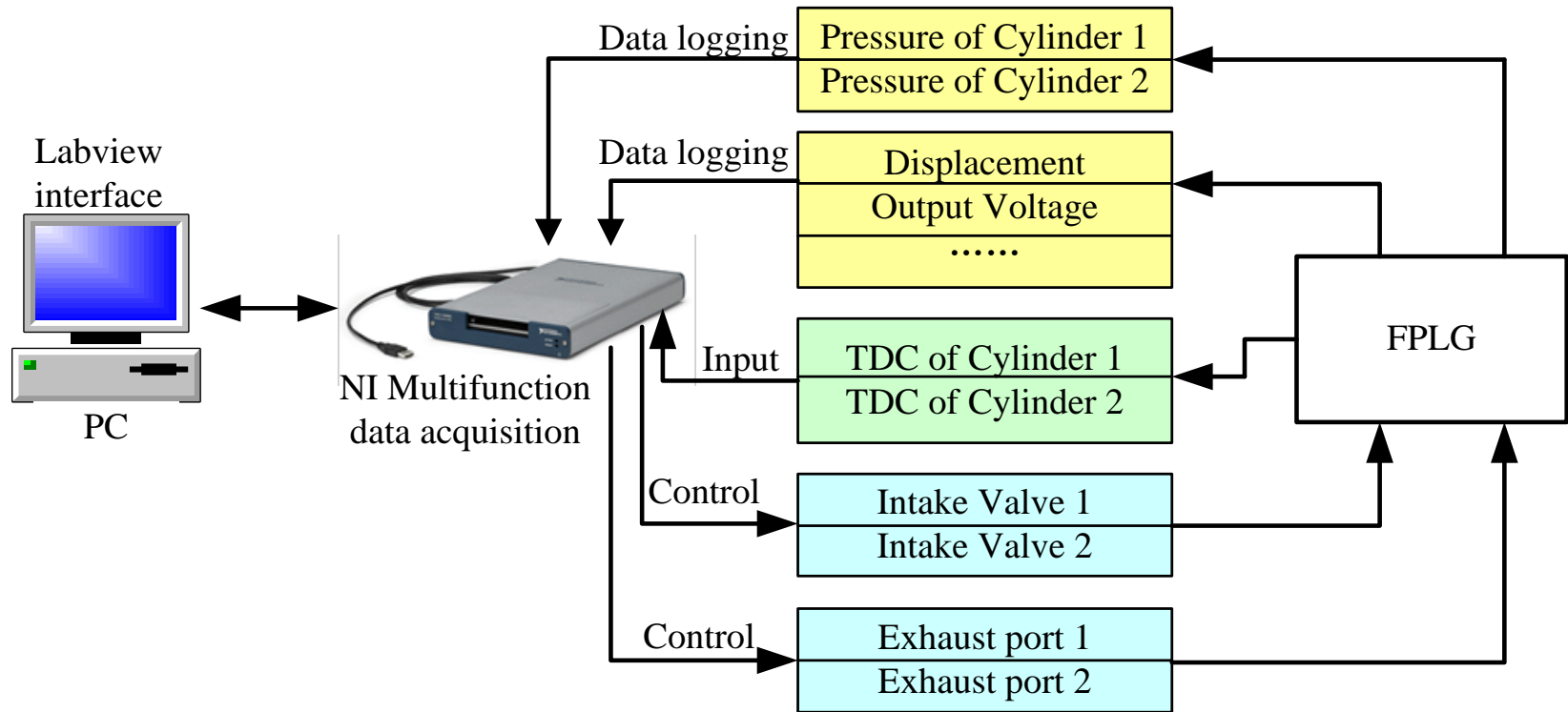


Strong mutual restricts between desorption and expansion

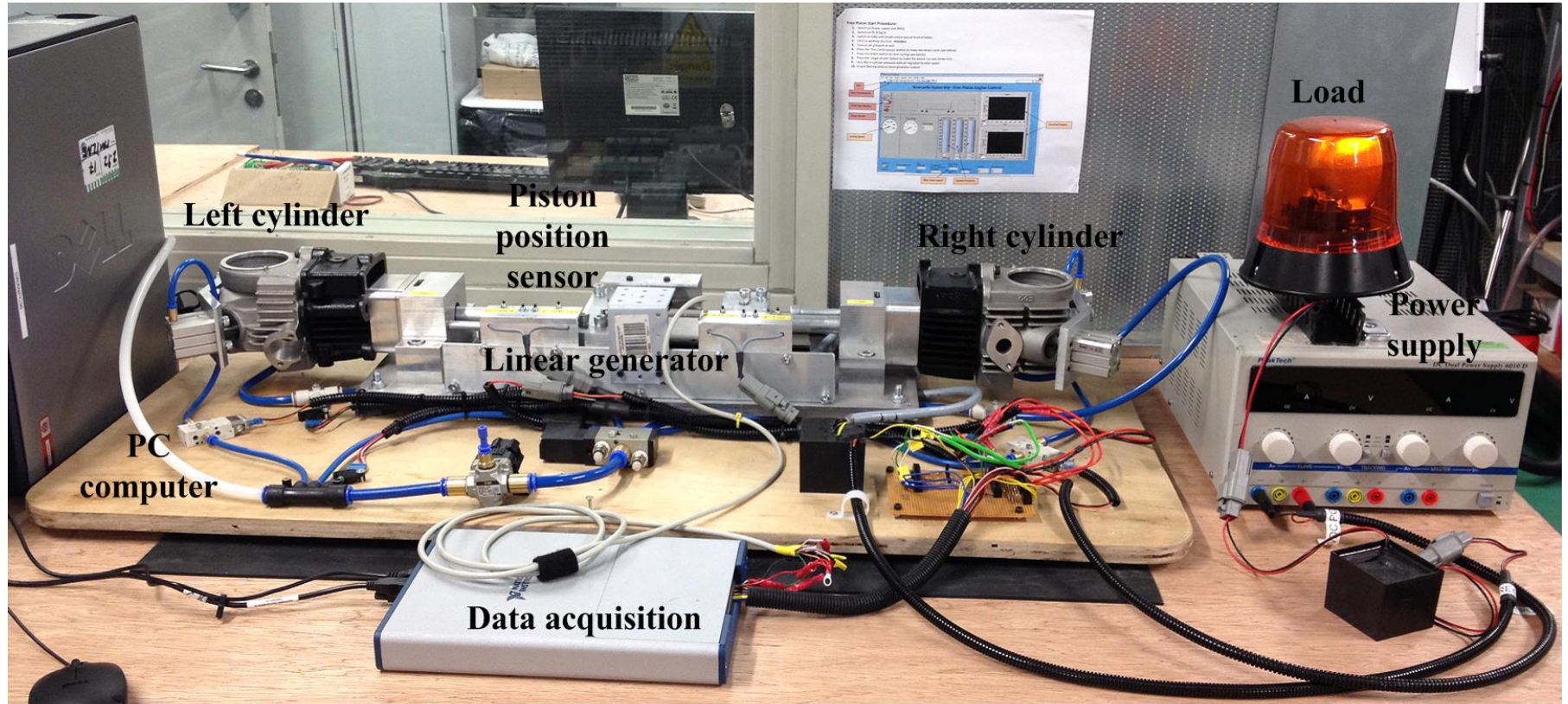
# Result: Cogeneration performance



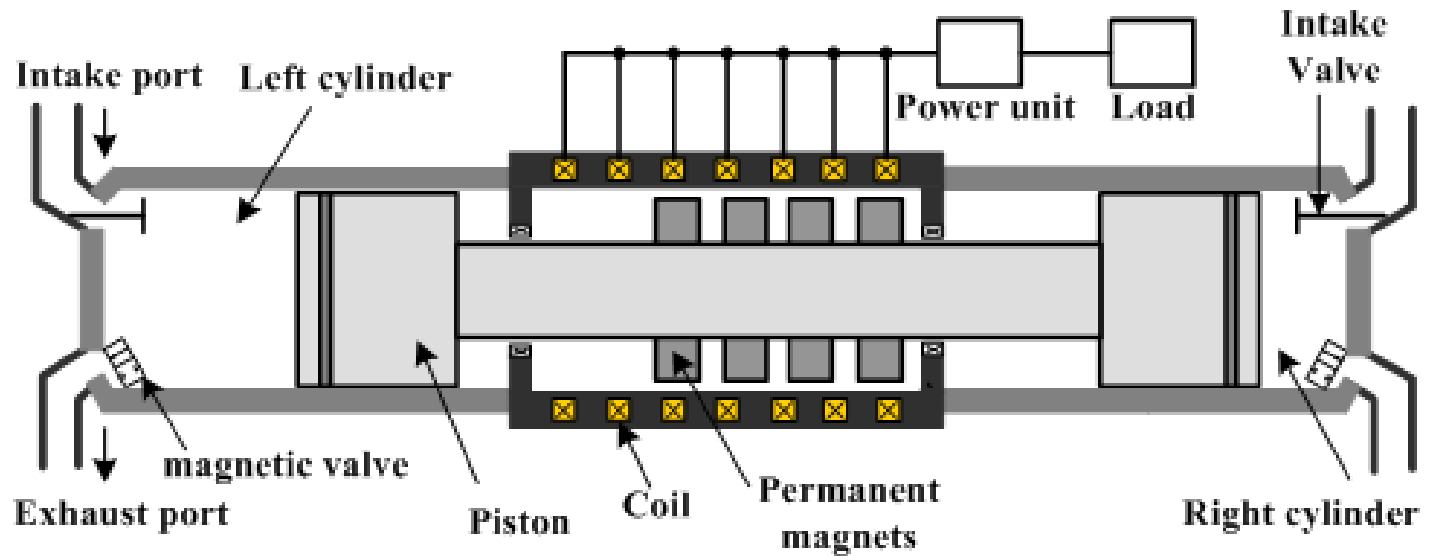
# Test rig of linear expander generator driven by compressed air (1)



# Prototype of linear (free-piston) generator test rig (2)

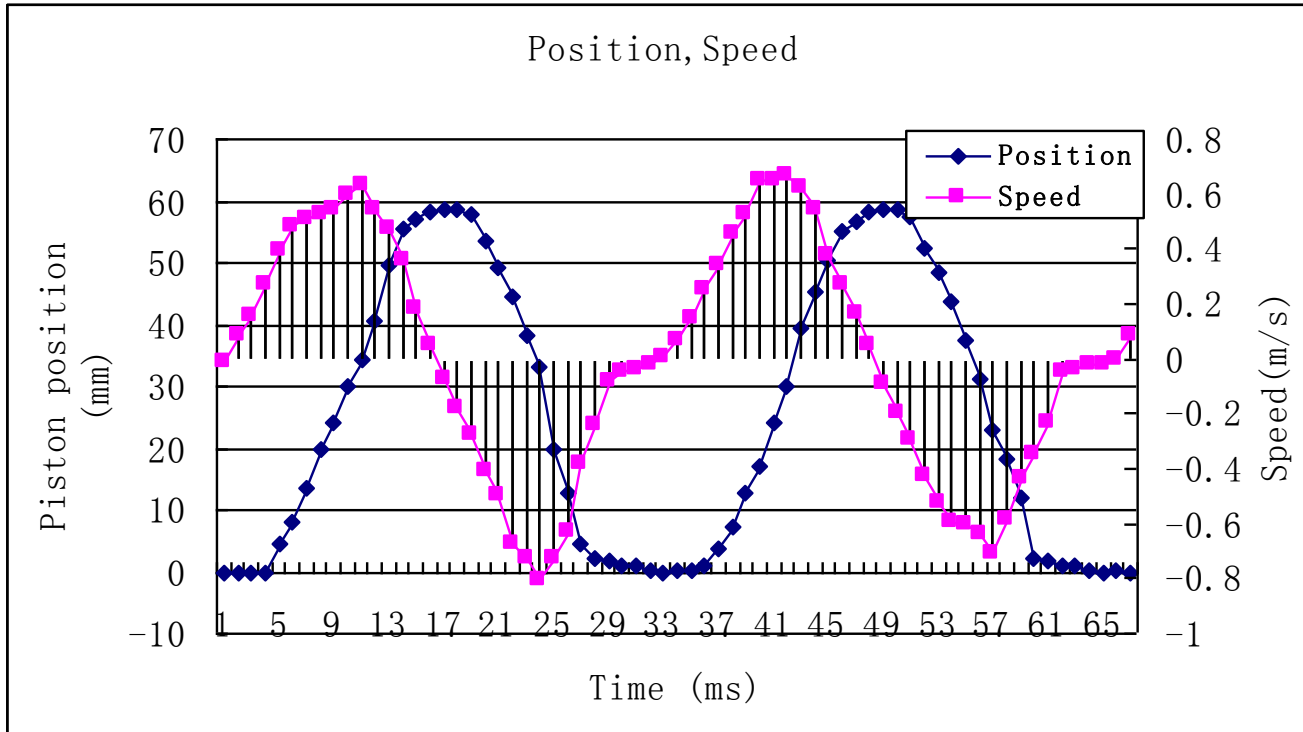


# Schematic diagram of linear expander generator

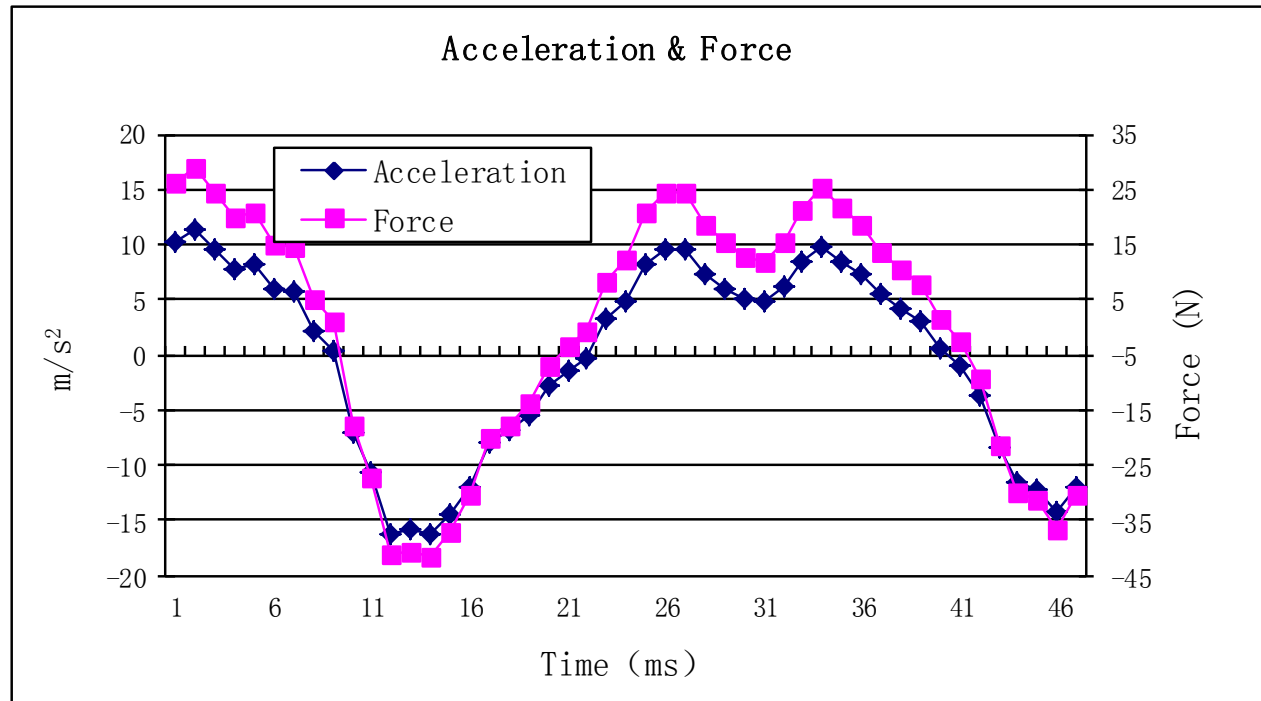




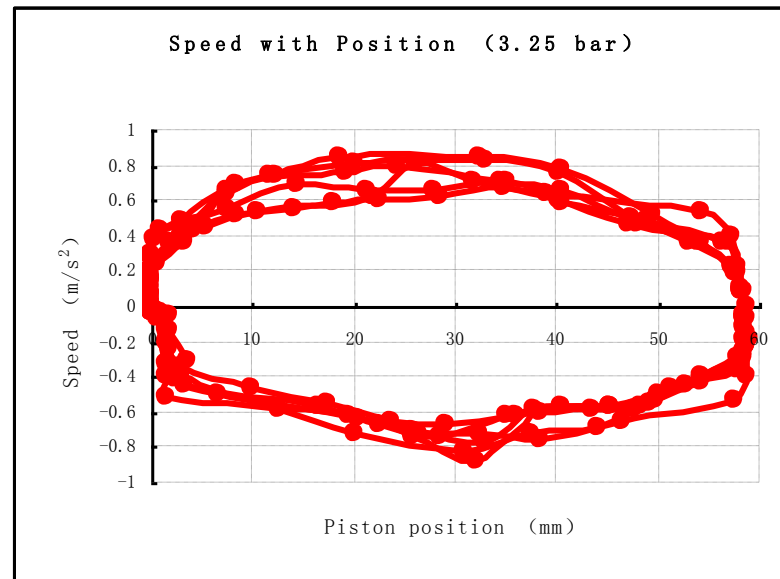
# Test results of linear expander generator driven by compressed air



# Test results of linear expander generator driven by compressed air

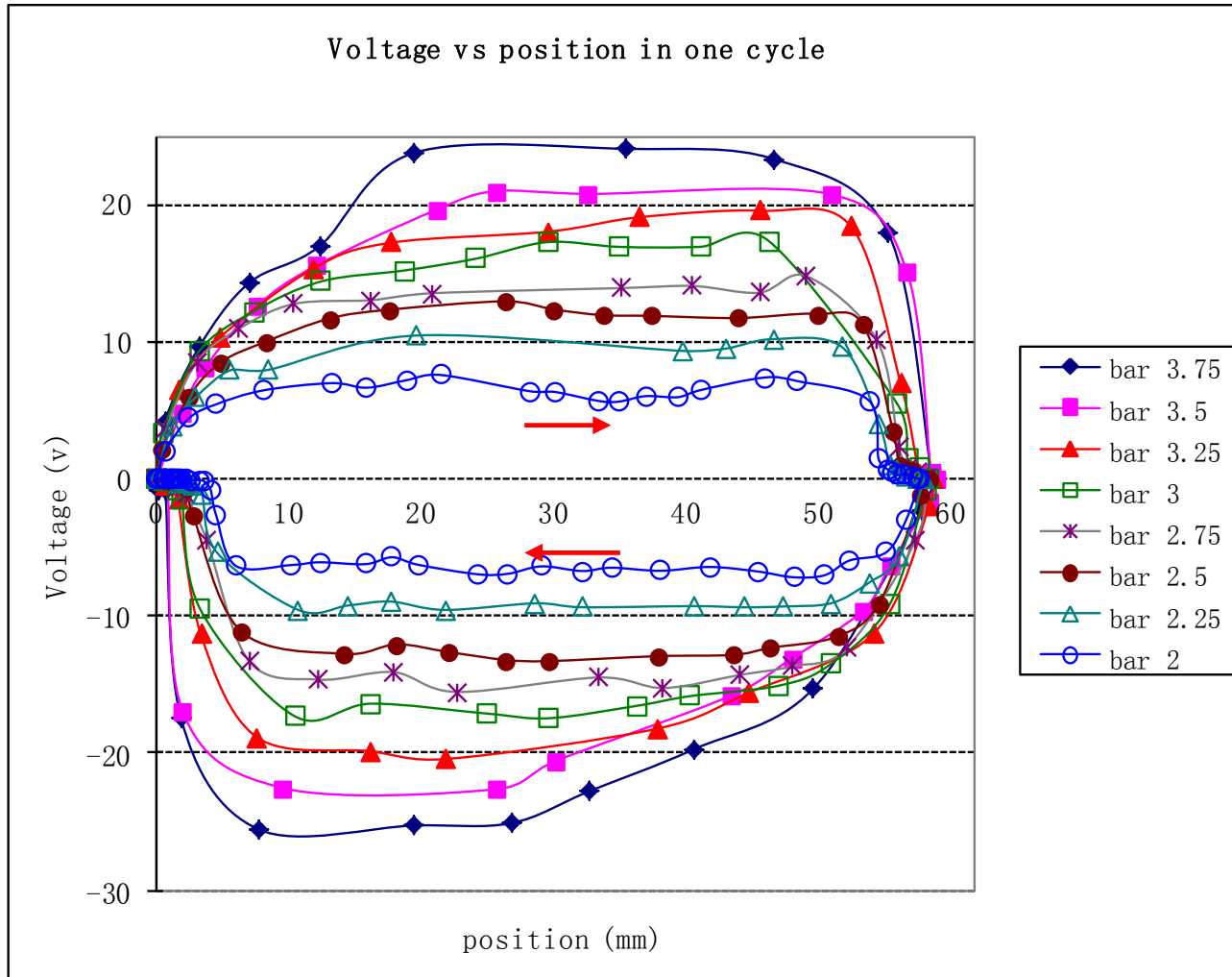


# Test results of linear expander generator driven by compressed air

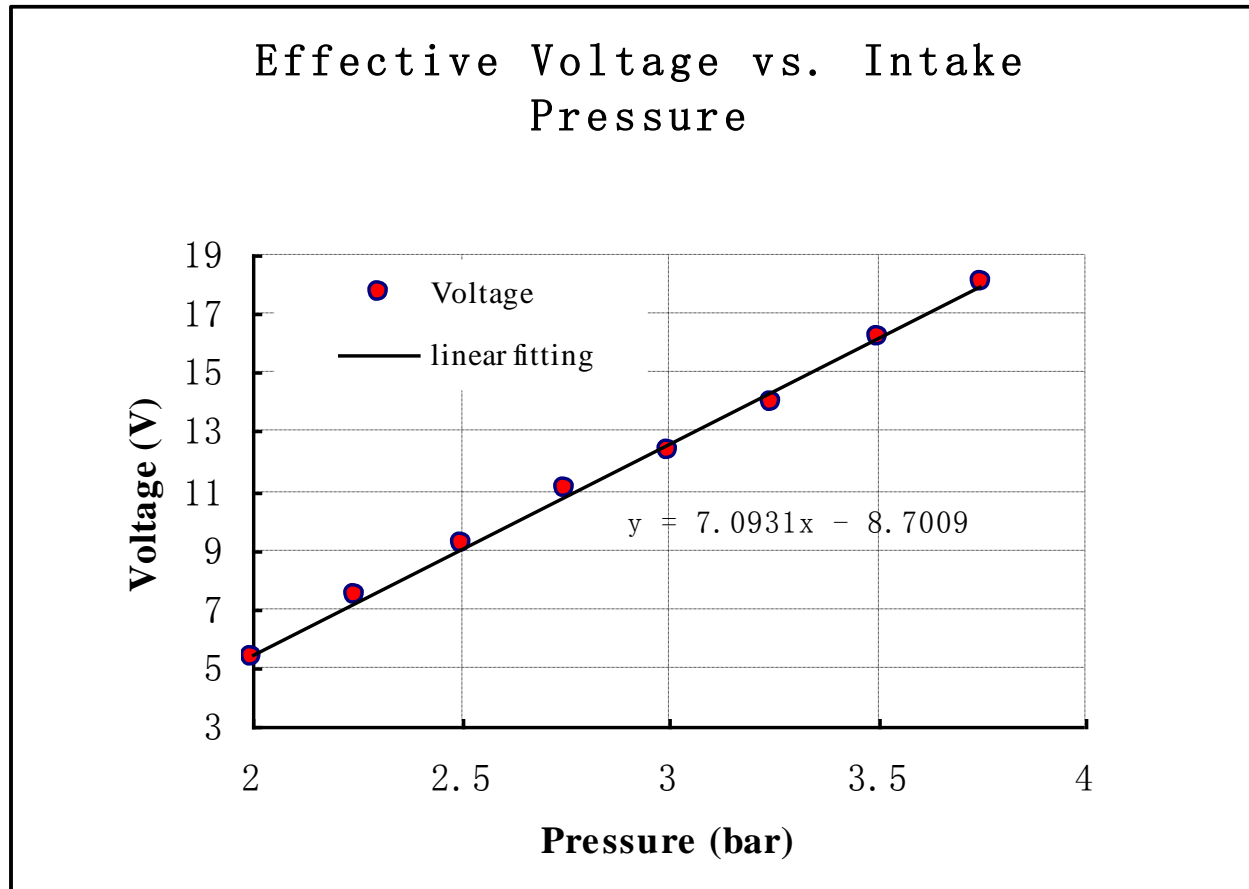


Piston velocity as a function of piston position at steady running condition.  
(pressure 3.25 bar)

# Test results of linear expander generator driven by compressed air



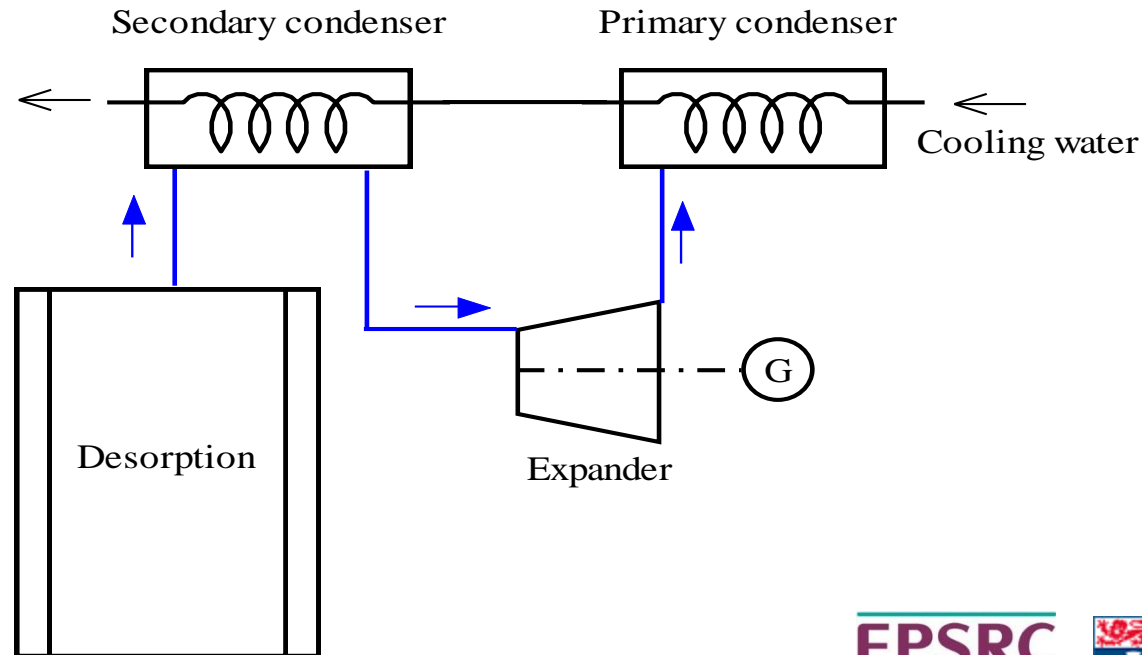
# Test results of linear expander generator driven by compressed air



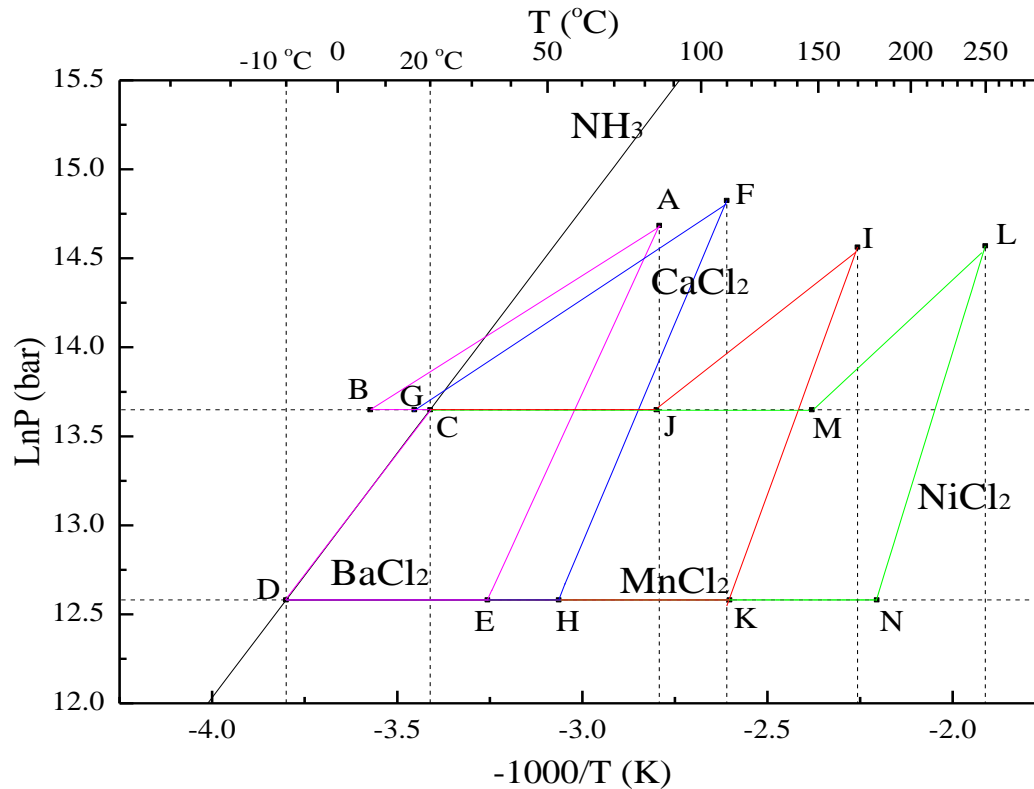
## 4. Improvement and potential application

### Improved design

A possible solution may mitigate or even eliminate the mutual restricts between the decomposition in reaction bed and the expansion process in the expander

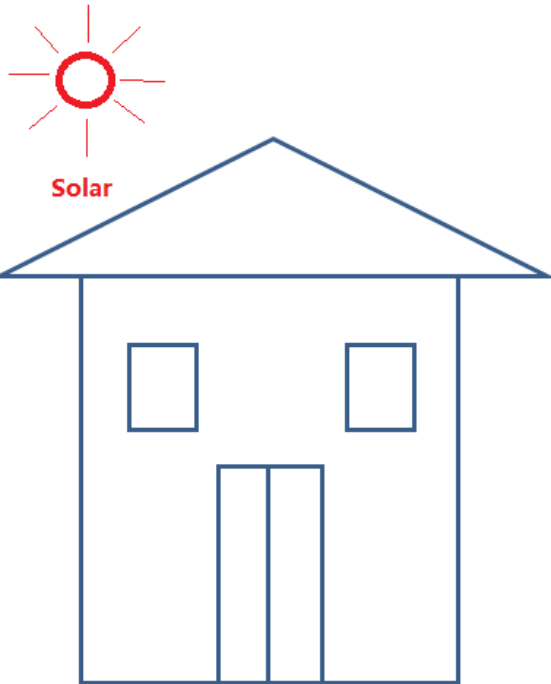


# Potential reactive materials



Salt complexes	Desorption temperature ( $^{\circ}\text{C}$ )	Desorption pressure (MPa)	Reaction enthalpy $\Delta H$ ( $\text{J/mol}(\text{NH}_3)$ )	COP	Exergy efficiency	
					Power	Refrigeration
$\text{BaCl}_2$ (8-0 $\text{NH}_3$ )	85.2	2.4	37665	0.57	0.39	0.23
$\text{CaCl}_2$ (8-4 $\text{NH}_3$ )	106	2.4	41013	0.41	0.24	0.13
$\text{MnCl}_2$ (6-2 $\text{NH}_3$ )	174.8	2.4	47416	0.42	0.19	0.089
$\text{NiCl}_2$ (6-2 $\text{NH}_3$ )	255	2.4	56160	0.34	0.14	0.056

# Potential applications



Biomass

Small scale household systems combined with biomass boiler / solar thermal units

or



Utilizing abundant waste heat in industries



## 5. Conclusions

- The adsorption cogeneration concept has been demonstrated and the viability has been preliminarily proven.
- The major challenge is the mutual restricts between the desorption process and the expansion process of the expander.
- Both linear expander and scroll expander are working driven by gases (air or ammonia ).
- The contradiction between the mountain-shaped desorption rate and the stable inlet required by power generation.
- Better refrigeration capacity than absorption-basis cogeneration technologies.

# Future Work

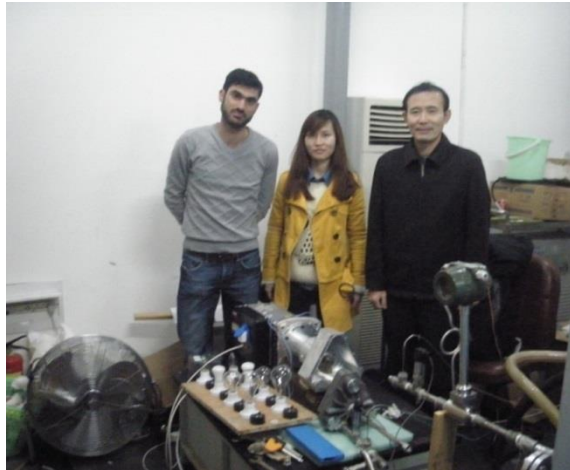
- Different complex salts may be considered for different refrigeration levels.
- An advanced system could be developed with a secondary condenser potentially can be used to mitigate the above problems.
- Due to the unsteady output, an energy storage unit may be added to the LH Cogen, using electricity storage devices such as batteries and supercapacitors.
- Further tests on linear expander using NH<sub>3</sub> is necessary, when funding available to build a new unit using materials adaptable/suitable for NH<sub>3</sub>.
- Re-design, manufacture and optimise the LH Cogen system including the adsorption unit, the linear expander.
- Further field tests using different low grade heat sources.

# Acknowledgement

This research outcome is from the research projects funded by Engineering and Physical Sciences Research Council (**EPSRC**):

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# Thank You!



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